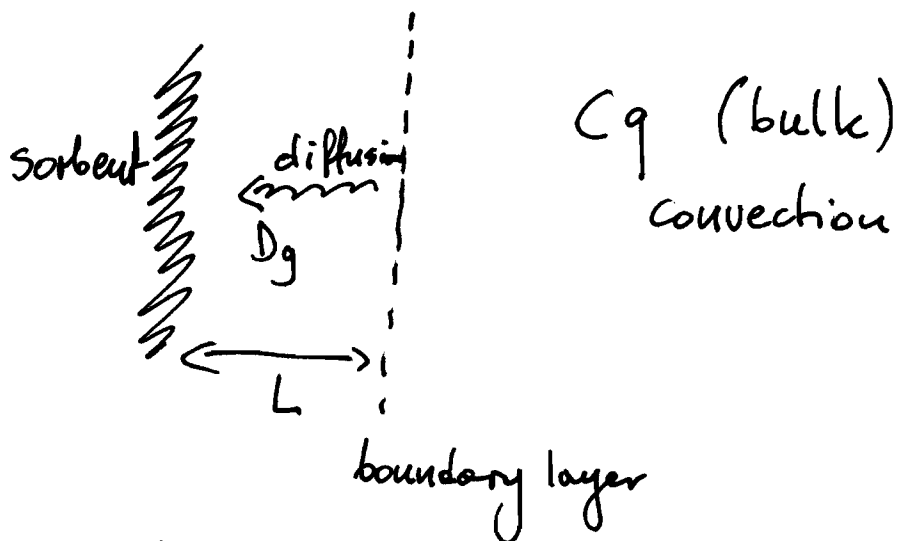


Homework on passive samplers

①



Where: flux into the sorbent $J = \frac{m}{A t}$

m (mass)

A (surface area of the sorbent face)

t (time)

assumption

- sorbent surface serves as zero sink for sample gas
- no competitive adsorption
- Fick's law describes the sampling process

$$J = - D_g \frac{dC_g}{dx}$$

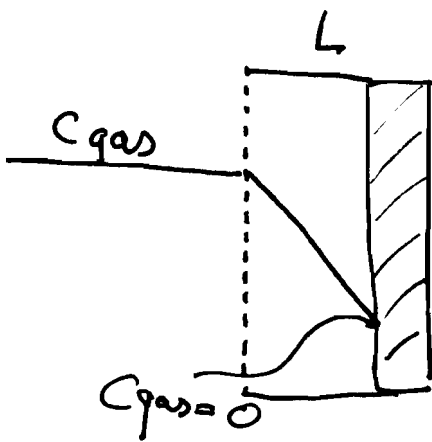
D_g - gas-phase diffusion coeff.

$$J dx = - D_g dC_g$$

$$J \int_0^L dx = - D_g \int_{C_g}^0 dC_g$$

$$J L = D_g C_g \rightarrow \bar{C}_g = \frac{J L}{D_g} = \boxed{\frac{m L}{A D_g t}}$$

(2)



linear process

$$C_g = \left(\frac{n}{A D_g t} \right) L$$

Problem 2

$t = 8 \text{ hrs} = 28,800 \text{ s}$ D_g for benzene @ room temp $\approx 0.09 \frac{\text{cm}^2}{\text{s}}$

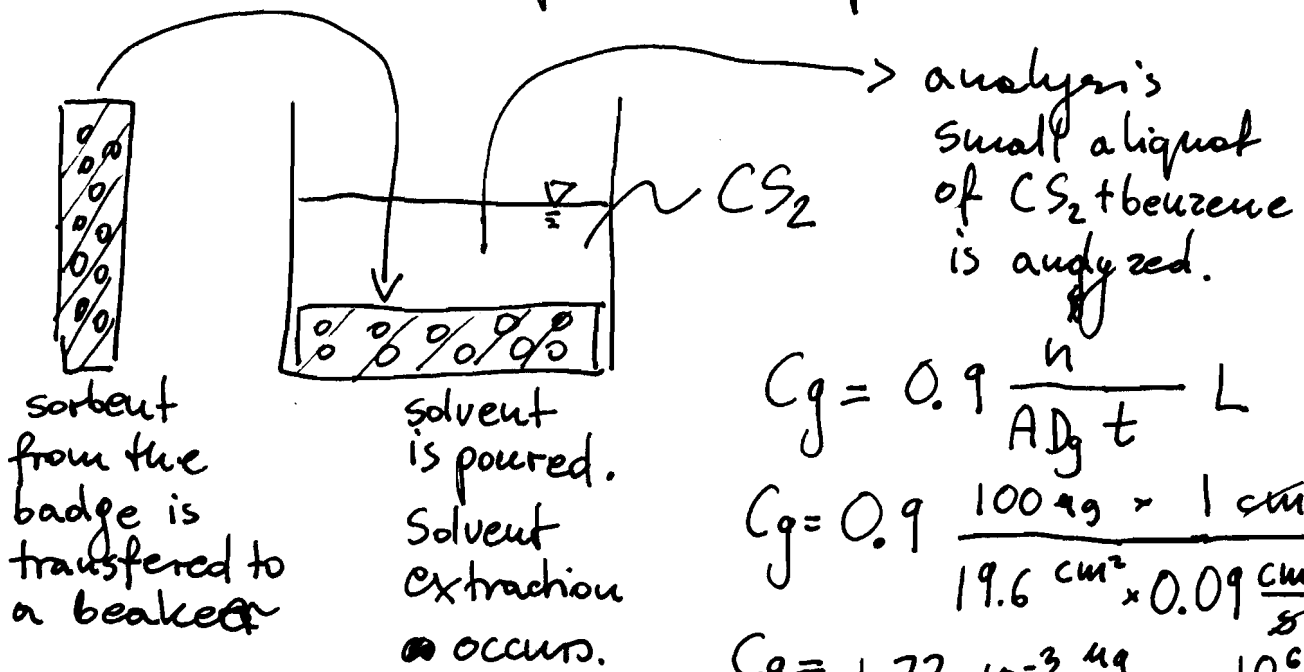
$L = 1 \text{ cm}$

$D = 5 \text{ cm}$

$n = 100 \text{ } \mu\text{g}$

$$A = \pi \left(\frac{5 \text{ cm}}{2} \right)^2 = 19.6 \text{ cm}^2$$

10% contribution of benzene from the solvent



$$C_g = 0.9 \frac{n}{A D_g t} L$$

$$C_g = 0.9 \frac{100 \text{ } \mu\text{g} \times 1 \text{ cm}}{19.6 \text{ cm}^2 \times 0.09 \frac{\text{cm}^2}{\text{s}} \times 28,800 \text{ s}}$$

$$C_g = 1.77 \times 10^{-3} \frac{\mu\text{g}}{\text{cm}^3} \times \frac{10^6 \text{ cm}^3}{\text{m}^3}$$

$$C_g = 1.77 \times 10^3 \frac{\mu\text{g}}{\text{m}^3} \approx 0.554 \text{ ppm}$$